

Energy-SmartOps

Integrated Control and Operation of Process, Rotating Machinery and Electrical Equipment

"Aerodynamic Impact of Fouling in Centrifugal Compressors"

Maria Esperanza Barrera-Medrano (ESR-F)

Mechanical Engineering Department, Thermofluids Division. Imperial College London

Fouling Phenomena

Fouling is the build-up of material inside the compressor, normally on the stationary components

Common causes:

- Airborne salt
- Industrial pollution
- Internal oil leaks
- Coal, dust ingested

Fouling produces:

- Changes blade shape
- Increase in surface roughness
- Distortion of flow aerodynamics

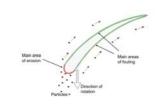
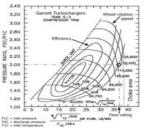


Figure 1. Compressor blade



Main Consequences

- Reduction in flow capacity
- Reduction in pressure ratio and efficiency
- Reduction in surge margin
- Stage degradation has a cumulative effect, making successive stages operate further away from their design point



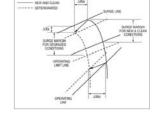


Figure 2. Compressor performance map example

Figure 3. Compressor performance map deterioration.

Research Aim

To construct a 1D, meanline, reduced order model for Centrifugal Compressors under Different Levels of Fouling

- To convert a clean, standard compressor performance map on to the equivalent map when the compressor operates with different inlet gas conditions.

Methodology Proposed

Compressor performance map generation under different levels of fouling [1].

Normalized method based on four nondimensional parameters at the design point to characterize the compressor performance:

- Flow coefficient, $oldsymbol{\phi}={}^{\dot{v}}\!/_{u_2D_2^2}$
- Tip-speed Mach number, $\mathbf{M} = {^{u_2}/a_1}$
- Work coefficient, $\lambda = \frac{\Delta h}{u_2^2}$
- Efficiency, η

Goal: To calculate the values of two dependent variables (η, λ) for specific values of independent variables (ϕ, M) :

$$\pmb{\eta}, \pmb{\lambda} = \mathrm{f} \left(\pmb{\phi}, \pmb{M} \right)$$

[1] M. Casey, C. Robinson, 2013. "A Method to Estimate the Performance Map of a Centrifugal Compressor Stage". ASME Journal of Turbomachinery, 135, p.021034

Methodology Proposed

Variation of **Efficiency** with **Flow** are based on: $\frac{\eta}{\eta_n} = f\left(M, \frac{\phi}{\phi_c}\right)$

Flows below the peak efficiency point $(\phi < \phi_p)$	Flows above the peak efficiency point $\left(\phi>\phi_{p} ight)$
$\frac{\eta}{\eta_p} = \left[1 - \left(1 - \frac{\phi/\phi_c}{\phi_p/\phi_c}\right)^D\right]^{1/p}$	$\frac{\eta}{\eta_p} = (1 - G) + G \left[1 - \left(\frac{\frac{\phi}{\phi_C} \frac{\phi_D}{\phi_C}}{1 - \frac{\phi_D}{\phi_C}} \right)^H \right]^{1/H}$

D, G and H are parameters that describe the stage characteristics

Variation of Work Input Coefficient with Flow and Tip-speed Mach number based on:

$$\lambda_{Euler} = \frac{c_{u2}}{u_2} = 1 - \frac{c_s}{u_2} + \phi_2 tan\beta_2'$$

 λ_{Euler} in terms of Inlet Flow Coefficient

n terms of **inlet Flow Coefficient**
$$\lambda_{Euler} = 1 - \frac{c_s}{u_2} + \frac{\phi D_2}{b_2 \pi} \frac{tan\beta_2'}{\left[1 + (\gamma - 1)\gamma_d \lambda M^2\right]^{\overline{n_d} - 1}}$$

 $L_{M2} = -NOS$ - NEAD $L_{M2} = -NOS$ - NEA

Future Work

- Experimental quantification of the performance deterioration due to fouling phenomena by experimental tests carried out on a centrifugal
- Quantification of the performance deterioration due to fouling by a validated performance prediction tool based on the methodology proposed.
- · Understanding the impact of fouling and process for the deterioration of
- This will enable energy savings by an estimation of cleaning schedules, replacement and load sharing.



Figure 4. MHI Centrifugal Compressor that will be tested.

Supervisor: Prof. Ricardo Martinez-Botas Mechanical Engineering Department, Thermofluids Division Imperial College London







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