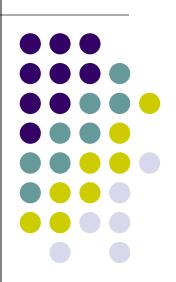
Introduction to Rheology of complex fluids Brief Lecture Notes

Nonlinear Viscoelasticity





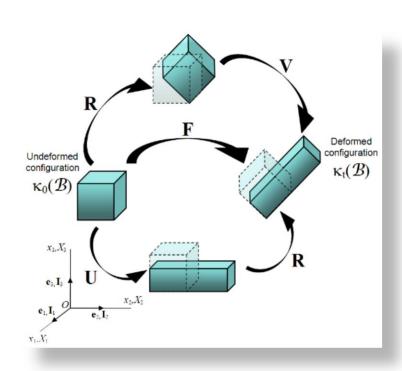
Contents

N=13

- Introductory Lecture
- Simple Flows
- Material functions & Rheological Characterization
- Experimental Observations
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- Generalized Linearly viscoelastic Fluids
- Nonlinear Constitutive Models



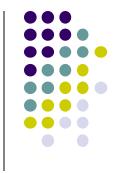




Nonlinear constitutive models: an overview



Macroscopic Constitutive models



$$\begin{aligned}
\underline{\tau} &= \underline{\tau} + \underline{\tau} \\
&= \underline{r} + \underline{\tau} \\
\underline{\tau} &= 2\eta_s \underline{\underline{D}} = \eta_s \dot{\underline{\gamma}}
\end{aligned}$$

$$\underline{\underline{\tau}} = \eta_s \dot{\underline{\gamma}} + b_2 \dot{\underline{\gamma}} + b_{11} \dot{\underline{\gamma}} \cdot \dot{\underline{\gamma}}$$

Second-order fluid

$$\underline{\underline{\tau}} + \lambda_{1} \underline{\underline{\tau}} + \lambda_{2} \left(\underline{\dot{\gamma}} \cdot \underline{\tau} + \underline{\underline{\tau}} \cdot \underline{\dot{\gamma}} \right) + \lambda_{3} tr(\underline{\underline{\tau}}) \underline{\dot{\gamma}} + \lambda_{4} \left(\underline{\underline{\tau}} : \underline{\dot{\gamma}} \right) \underline{\underline{I}} =$$

$$\eta_{o} \left(\underline{\dot{\gamma}} + \lambda_{5} \underline{\dot{\gamma}} + \lambda_{6} \underline{\dot{\gamma}} \cdot \underline{\dot{\gamma}} + \lambda_{7} \left(\underline{\dot{\gamma}} : \underline{\dot{\gamma}} \right) \underline{\underline{I}} \right)$$

Oldroyd 8constant



Macroscopic Constitutive models

$$\underline{\underline{\tau}} = \underline{\tau} + \underline{\tau}$$

$$\underline{\underline{\tau}} = p + \underline{\underline{\tau}}$$

$$\underline{\underline{\tau}} = 2\eta_s \underline{\underline{D}}$$

$$\underline{\underline{\tau}} = 2\eta_s \underline{\underline{D}}$$

$$\underline{\underline{\tau}} + \lambda \underline{\underline{\tau}} + \underline{\underline{F}} (\underline{\underline{D}}, \underline{\underline{\tau}}) = 2\eta_p \underline{\underline{D}}$$



 $\underline{\underline{F}}\left(\underline{\underline{D}},\underline{\tau}_{n}\right) = \underline{0}$

Johnson-Segalman

$$\underline{\underline{F}}\left(\underline{\underline{D}},\underline{\tau}_{p}\right) = \alpha\underline{\tau} \cdot \underline{\tau}_{p}$$

Giesekus

$$\underline{\underline{F}}\left(\underline{\underline{D}},\underline{\tau}_{=p}\right)$$

$$\underline{\underline{F}}\left(\underline{\underline{D}}, \underline{\tau}_{p}\right) = \alpha \underline{\underline{D}} : \underline{\tau}_{p} \left(\underline{\tau}_{p} + GI\right)$$



$$\underline{\underline{F}}\left(\underline{\underline{D}}, \underline{\tau}_{p}\right) = \underline{0} \qquad \lambda = G/\eta_{p}\left(\sqrt{\underline{\underline{D}} : \underline{\underline{D}}}\right)$$

$$\lambda = G/\eta_p\left(\sqrt{\underline{\underline{D}}:\underline{\underline{D}}}\right)$$

$$\eta_p = \eta_p \left(\sqrt{\underline{\underline{D}} : \underline{\underline{D}}} \right)$$



Macroscopic Constitutive models



$$\underline{\underline{\tau}} = \underline{\tau} + \underline{\tau} \\
\underline{\underline{\tau}} = 2\eta_s \underline{\underline{D}}$$

$$\underline{\underline{\tau}} + \lambda \underline{\underline{\tau}} + a \frac{\lambda}{\eta_p} \underline{\underline{\tau}} \cdot \underline{\underline{\tau}} = \eta_p \dot{\underline{\gamma}} \\
\underline{\underline{\tau}} = \eta_p \dot{\underline{\gamma}} = \eta_p \dot{\underline{\gamma}}$$

$$\underline{\tau}_{=p} + \lambda \underline{\tau}_{=p}^{\nabla} + a \frac{\lambda}{\eta_p} \underline{\tau}_{=p} \cdot \underline{\tau}_{=p} = \eta_p \dot{\underline{\gamma}}_{=p}$$

$$\underline{\tau}_{=p} + \lambda \underline{\tau}_{=p}^{\nabla} = \eta_p \dot{\underline{\gamma}} - \frac{2}{3} \lambda \left(\underline{\tau}_{=p} : \underline{\nabla}\underline{v}\right) \left(\underline{\underline{I}} + (1 + \varepsilon) \frac{\lambda}{\eta_p} \underline{\tau}_{=p}\right)$$

Rolie-Poly

$$\underline{\tau}_{p} + \lambda \left(\frac{\underline{\tau}_{p}}{f(\underline{\tau}_{p})} \right) = \frac{\eta_{p}}{f(\underline{\tau}_{p})} \dot{\underline{\tau}} - \eta_{p} \frac{D}{Dt} \left(\frac{1}{f(\underline{\tau}_{p})} \right) \underline{\underline{I}}$$

FENE-P

$$\frac{\tau}{z_{p}} + \lambda \left(\frac{\frac{\tau}{z_{p}}}{f(\frac{\tau}{z_{p}})} \right) = \eta_{p} \dot{\gamma}$$

$$f(\tau_{=p}) = 1 + \frac{\lambda}{\eta_p L^2} tr(\tau_{=p})$$



PTT models



$$\frac{\tau}{z} = 2\eta_s \underline{\underline{D}}$$

$$\frac{\tau}{z} = 2\eta_s \underline{\underline{D}}$$

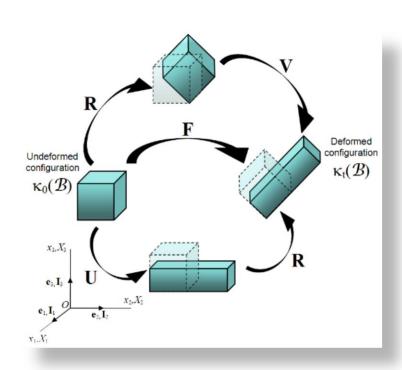
$$f\left(tr\tau_{z}\right) \tau_{z} + \lambda \left(\frac{D_{\xi z} \tau}{Dt}\right) = 2\eta_p \underline{\underline{D}}$$

$$f\left(tr\tau_{=p}\right) = \begin{cases} 1 + \frac{\varepsilon\lambda}{\eta_p} tr\left(\frac{\tau}{=p}\right) & \text{Linear PTT} \\ 1 + \frac{\varepsilon\lambda}{\eta_p} tr\left(\frac{\tau}{=p}\right) + \frac{1}{2}\left(\frac{\varepsilon\lambda}{\eta_p} tr\left(\frac{\tau}{=p}\right)\right)^2 & \text{Quadratic PTT} \\ \exp\left(\frac{\varepsilon\lambda}{\eta_p} tr\left(\frac{\tau}{=p}\right)\right) & \text{Exponential PT} \end{cases}$$

Exponential PTT







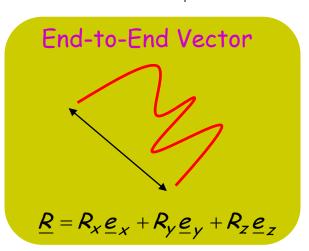
Conformation tensor <u>A</u>



Conformation Tensor: <u>A</u>=<<u>RR</u>>



$$\underline{A} = \underline{c} = \underline{r}\underline{r} = \langle \underline{R}\underline{R} \rangle = \begin{pmatrix} \langle R_x^2 \rangle & \langle R_x R_y \rangle & \langle R_x R_z \rangle \\ \langle R_y R_x \rangle & \langle R_y^2 \rangle & \langle R_y R_z \rangle \\ \langle R_z R_x \rangle & \langle R_z R_y \rangle & \langle R_z^2 \rangle \end{pmatrix}$$
Vector



The more complex the configuration of a polymer chain, the more non-zero entries in <u>A</u>

Spherical Symmetry

$$\underline{\underline{c}} = \begin{pmatrix} \left\langle \mathbf{R}_{x}^{2} \right\rangle & 0 & 0 \\ 0 & \left\langle \mathbf{R}_{x}^{2} \right\rangle & 0 \\ 0 & 0 & \left\langle \mathbf{R}_{x}^{2} \right\rangle \end{pmatrix}$$

Cylindrical Symmetry
$$\underline{\underline{c}} = \begin{pmatrix} \langle \mathcal{R}_{x}^{2} \rangle & 0 & 0 \\ 0 & \langle \mathcal{R}_{y}^{2} \rangle & (\neq \langle \mathcal{R}_{x}^{2} \rangle) & 0 \\ 0 & 0 & \langle \mathcal{R}_{z}^{2} \rangle & (\neq \langle \mathcal{R}_{x}^{2} \rangle) \end{pmatrix}$$







$$\tau_{=\rho} = G\underline{A}$$

$$\underline{\tau}_{=\rho} = \mathcal{G}\left(\underline{\underline{A}} - \underline{\underline{I}}\right)$$

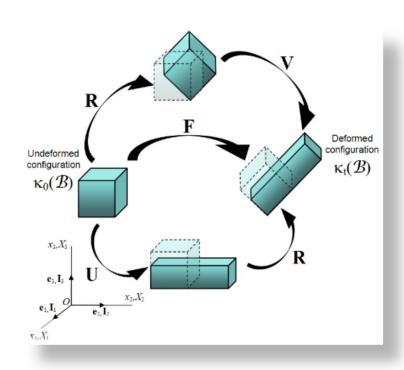
$$G = nk_BT$$

The stress components are proportional to the 3D chain configuration. *G* is the shear modulus.

But we have to define a reference (undeformed=random) state: <u>A=I</u>







Rheological Characterization Oldroyd-B



The constitutive model: Oldroyd-B



In conformation tensor form

$$\tau_{=p} = G\underline{A} \tag{1}$$

$$\frac{\partial \mathbf{A}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{A} - \mathbf{A} \cdot \nabla \mathbf{v} - (\nabla \mathbf{v})^T \cdot \mathbf{A} = -\frac{1}{\lambda} (\mathbf{A} - \mathbf{I})$$
 (2)

To express the constitutive relation in terms of stresses, eq. (1) should be solved in terms of conformation tensor \underline{A} (= \underline{c}) and substituted in eq. (2).



Governing equations for the flow of an Oldroyd-B fluid



$$\underline{\nabla} \cdot \underline{\boldsymbol{\nu}} = 0$$

$$\rho \left(\frac{\partial \underline{\boldsymbol{\nu}}}{\partial \boldsymbol{\tau}} + \underline{\boldsymbol{\nu}} \cdot \underline{\nabla} \underline{\boldsymbol{\nu}} \right) = \underline{\nabla} \cdot \underline{\boldsymbol{\tau}}$$

$$\underline{\tau} = -p\underline{\underline{I}} + \eta_{s} ((\underline{\nabla v}) + (\underline{\nabla v})^{T}) + \underline{\tau}_{=p}$$

$$\tau_{=p} = GA$$

$$\frac{\partial \mathbf{A}}{\partial t} + (\mathbf{v} \cdot \nabla) \mathbf{A} - \mathbf{A} \cdot \nabla \mathbf{v} - (\nabla \mathbf{v})^{T} \cdot \mathbf{A} = -\frac{1}{\lambda} (\mathbf{A} - \mathbf{I})$$

Equations for the complete determination of both the velocity and the stress fields



Simple Shear Flow



Let the velocity field equal to

$$\underline{v}(y,t) = (\dot{\varsigma}(t)y,0,0)$$

$$\underline{\nabla}\underline{v}(y,t) = \begin{pmatrix} 0 & 0 \\ \dot{\varsigma}(t) & 0 \end{pmatrix}$$

The total stress tensor is given by the relation

$$\tau = \begin{pmatrix} -p & \eta_s \dot{\varsigma}(t) \\ \eta_s \dot{\varsigma}(t) & -p \end{pmatrix} + GA = 0$$

The viscoelastic stresses are

$$\underline{\tau}_{p} = G\underline{A}$$

The conformation tensor is determined by

$$\frac{\partial}{\partial t} \begin{pmatrix} A_{xx} & A_{xy} \\ A_{yx} & A_{yy} \end{pmatrix} - \begin{pmatrix} \dot{\varsigma}(t)A_{xy} & 0 \\ \dot{\varsigma}(t)A_{yy} & 0 \end{pmatrix} - \begin{pmatrix} \dot{\varsigma}(t)A_{xy} & \dot{\varsigma}(t)A_{yy} \\ 0 & 0 \end{pmatrix} = -\frac{1}{\lambda} \begin{pmatrix} A_{xx} - 1 & A_{xy} \\ A_{yx} & A_{yy} - 1 \end{pmatrix}$$



Steady Simple Shear Flow



The viscoelastic stress is

$$\tau_{=p} = G \begin{pmatrix} A_{xx} & A_{xy} \\ A_{yx} & A_{yy} \end{pmatrix}$$

And the conformation tensor is

$$-\begin{pmatrix} \dot{\gamma}_o A_{xy} & 0 \\ \dot{\gamma}_o A_{yy} & 0 \end{pmatrix} - \begin{pmatrix} \dot{\gamma}_o A_{xy} & \dot{\gamma}_o A_{yy} \\ 0 & 0 \end{pmatrix} = -\frac{1}{\lambda} \begin{pmatrix} A_{xx} - 1 & A_{xy} \\ A_{yx} & A_{yy} - 1 \end{pmatrix}$$



Steady Simple Shear Flow



Which results into

$$\begin{cases} A_{yy} = 1 \\ A_{xy} = \dot{\gamma}_o \lambda \\ A_{xx} = 1 + 2\dot{\gamma}_o^2 \lambda^2 \end{cases}$$

$$\underline{\underline{\tau}}_{p} = G \begin{pmatrix} A_{xx} & A_{xy} \\ A_{yx} & A_{yy} \end{pmatrix} = G \begin{pmatrix} 1 + 2\dot{\gamma}_{o}^{2}\lambda^{2} & \dot{\gamma}_{o}\lambda \\ \dot{\gamma}_{o}\lambda & 1 \end{pmatrix}$$

The total stress tensor

$$\underline{\tau} = \begin{pmatrix} -p + G + 2G\dot{\gamma}_o^2\lambda^2 & (\eta_s + G\lambda)\dot{\gamma}_o \\ (\eta_s + G\lambda)\dot{\gamma}_o & -p + G \end{pmatrix}$$





$$\eta = \eta_s + G\lambda$$

The First Normal Stress Difference is:

$$N_1(\dot{\gamma}_o) = \tau_{xx} - \tau_{yy} = 2G\lambda^2 \dot{\gamma}_o^2$$









Oscillatory Simple Shear Flow (SAOS)

The conformation tensor is given by

$$\frac{\partial}{\partial t} \begin{pmatrix} A_{xx} & A_{xy} \\ A_{yx} & A_{yy} \end{pmatrix} - \begin{pmatrix} \dot{\varsigma}(t)A_{xy} & 0 \\ \dot{\varsigma}(t)A_{yy} & 0 \end{pmatrix} - \begin{pmatrix} \dot{\varsigma}(t)A_{xy} & \dot{\varsigma}(t)A_{yy} \\ 0 & 0 \end{pmatrix} = -\frac{1}{\lambda} \begin{pmatrix} A_{xx} - 1 & A_{xy} \\ A_{yx} & A_{yy} - 1 \end{pmatrix}$$

The rate of deformation equals

$$\dot{\varsigma}(t) = \alpha\omega\cos(\omega t)$$





$$\underline{\underline{A}} = \underline{\underline{I}}$$

A = I All the chains are initially unstretched

By integrating in time we have

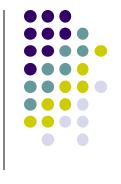
$$\frac{\partial A_{yy}}{\partial t} = -\frac{1}{\lambda} \left(A_{yy} - 1 \right)$$

Which gives $A_{vv} = 1$

$$\frac{\partial A_{xy}}{\partial t} - \dot{\varsigma}(t) A_{yy} = -\frac{1}{\lambda} A_{xy}$$



$$\frac{\partial A_{xy}}{\partial t} - \alpha \omega \cos(\omega t) = -\frac{1}{\lambda} A_{xy}$$
$$\frac{\partial A_{xy}}{\partial t} + \frac{1}{\lambda} A_{xy} = \alpha \omega \cos(\omega t)$$
$$\frac{\partial}{\partial t} \left(A_{xy} e^{t/\lambda} \right) = \alpha \omega \cos(\omega t) e^{t/\lambda}$$





Thus,

$$A_{xy} = \frac{1}{1 + \omega^2 \lambda^2} \left(\alpha \omega \lambda \cos(\omega t) + \alpha \omega^2 \lambda^2 \sin(\omega t) - \alpha \omega \lambda e^{-t/\lambda} \right)$$



For
$$t \to \infty$$
 $e^{-t/\lambda} << 1$

$$\tau_{xy} = \left(\eta_s + \frac{G\lambda}{1 + \omega^2 \lambda^2}\right) \dot{\gamma}(t) + \frac{G\omega^2 \lambda^2}{1 + \omega^2 \lambda^2} \gamma(t)$$

$$G'(\omega) = \frac{G\omega^2\lambda^2}{1 + \omega^2\lambda^2}$$

$$G''(\omega) = \eta_s + \frac{G\lambda}{1 + \omega^2 \lambda^2}$$



Steady 2D Extensional Flow



Let the velocity field be

$$\underline{v}(y,t) = (\dot{\varepsilon}_o x, -\dot{\varepsilon}_o y)$$

$$\underline{\nabla}\underline{v}(y,t) = \begin{pmatrix} \dot{\varepsilon}_o & 0\\ 0 & -\dot{\varepsilon}_o \end{pmatrix}$$

The total stress tensor is given by the relation

$$\underline{\tau} = \begin{pmatrix} -p + 2\eta_s \dot{\varepsilon}_o & 0 \\ 0 & -p - 2\eta_s \dot{\varepsilon}_o \end{pmatrix} + G\underline{A}$$

The viscoelastic stresses are

$$\tau_{=p} = G\underline{A}$$

The conformation tensor

$$-\begin{pmatrix} \dot{\varepsilon}_{o}A_{xx} & -\dot{\varepsilon}_{o}A_{xy} \\ \dot{\varepsilon}_{o}A_{xy} & -\dot{\varepsilon}_{o}A_{yy} \end{pmatrix} - \begin{pmatrix} \dot{\varepsilon}_{o}A_{xx} & \dot{\varepsilon}_{o}A_{xy} \\ -\dot{\varepsilon}_{o}A_{xy} & -\dot{\varepsilon}_{o}A_{yy} \end{pmatrix} = -\frac{1}{\lambda}\begin{pmatrix} A_{xx} - 1 & A_{xy} \\ A_{yx} & A_{yy} - 1 \end{pmatrix}$$



$$A_{xx} = \frac{1}{1 - 2\dot{\varepsilon}_o \lambda}$$

$$A_{xy} = 0$$

$$A_{yy} = \frac{1}{1 + 2\dot{\varepsilon}_o \lambda}$$

Hence,

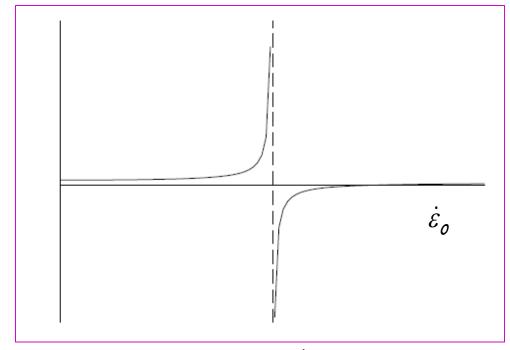
$$A_{yy} = \frac{1}{1 + 2\dot{\varepsilon}_o \lambda}$$

The extensional Viscosity $\eta_e = \frac{\tau_{xx} - \tau_{yy}}{4\dot{\epsilon}}$





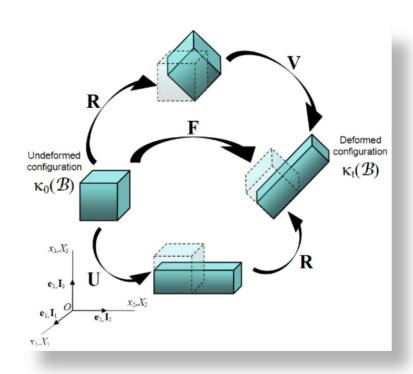
$$\eta_e = \eta + \frac{G\lambda}{1 - 4\dot{\varepsilon}_o \lambda^2}$$



$$\dot{\varepsilon}_o = \frac{1}{2\lambda}$$







Giesekus Model



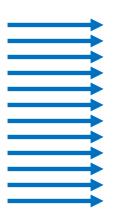
Anisotropic Drag Force

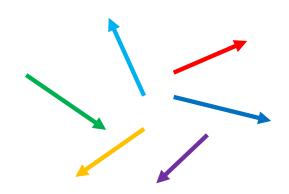


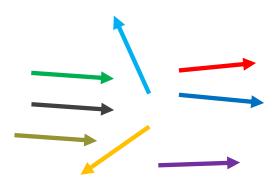
Flow field

Isotropy in chain mobility

Anisotropy in chain mobility

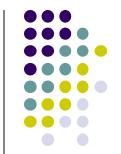




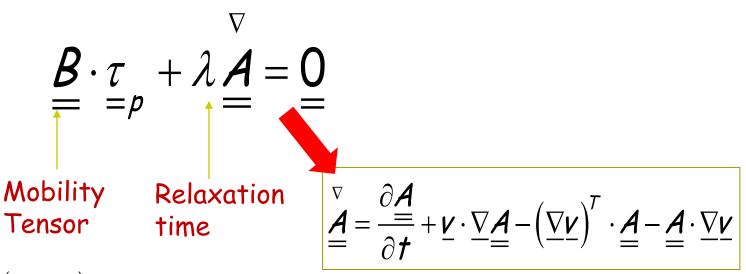




Anisotropic Drag Force



When a system is deformed, the space where a macromolecule deforms becomes anisotropic. This will lead to anisotropic drag force on it.



$$\underline{\underline{B}} = \underline{\underline{I}} + a(\underline{\underline{A}} - \underline{\underline{I}})$$

a is a parameter that determines the degree of anisotropy in chain mobility



The constitutive model in terms of conformation tensor



3-Constant Giesekus model. Relation is expressed in terms of the conformation tensor

$$a\left(\underline{\underline{A}} - \underline{\underline{I}}\right)^{2} + \left(\underline{\underline{A}} - \underline{\underline{I}}\right) + \lambda \underline{\underline{A}} = \underline{\underline{0}}$$

$$\tau_{=\rho} = \mathcal{G}\left(\underbrace{\underline{\mathcal{A}} - \underline{I}}_{=}\right)$$



The constitutive model in terms of stress tensor

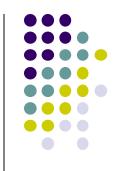


3-Constant Giesekus model. Here expressed in terms of the polymeric stress tensor

$$\underline{\tau}_{=\rho} + \lambda \underline{\tau}_{=\rho}^{\nabla} + \mathbf{a} \frac{\lambda}{\eta_o} \underline{\tau}_{=\rho} \cdot \underline{\tau}_{=\rho} = \eta_o \dot{\underline{\gamma}}_{=\rho}$$







Steady Shear Flow

$$\frac{\eta}{\eta_o} = \frac{(1-f)^2}{1+(1-2a)f}$$

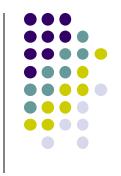
$$\frac{\Psi_1}{2\eta_o\lambda} = \frac{f(1-af)}{(1-f)a} \frac{1}{(\lambda \dot{\gamma}_o)^2}$$

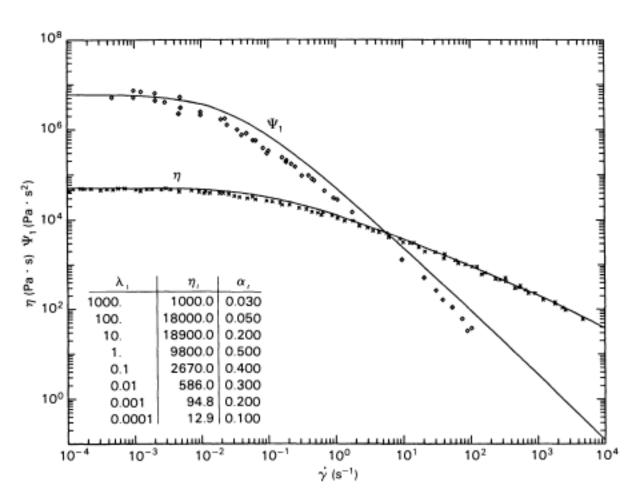
$$\frac{\Psi_2}{\eta_o \lambda} = -f \frac{1}{(\lambda \dot{\gamma}_o)^2}$$

$$f = \frac{1-\chi}{1+(1-2a)\chi}$$

where
$$f = \frac{1-\chi}{1+(1-2a)\chi}$$
 $\chi^2 = \frac{\left[1+16a(1-a)(\lambda\dot{\gamma}_o)^2\right]^{1/2}-1}{8a(1-a)(\lambda\dot{\gamma}_o)^2}$







Viscosity and first normal stress coefficient for an 8-mode Giesekus model as compared to experimental data for a low-density polyethylene melt







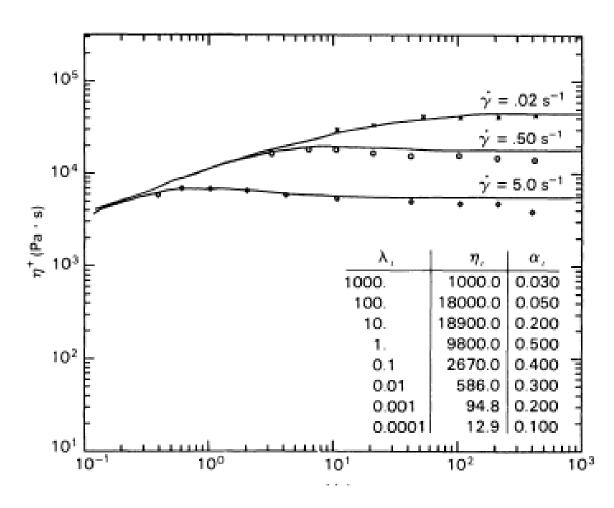
Small Amplitude Oscillatory Flow

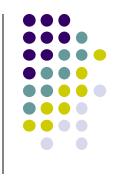
$$\frac{\eta'}{\eta_o} = \frac{1}{1 + (\lambda \omega)^2}$$

$$\frac{\eta''}{\eta_o} = \frac{\lambda \omega}{1 + (\lambda \omega)^2}$$









Comparison of n+ calculated by an 8-mode Giesekus model with experimental data for a low-density polyethylene melt







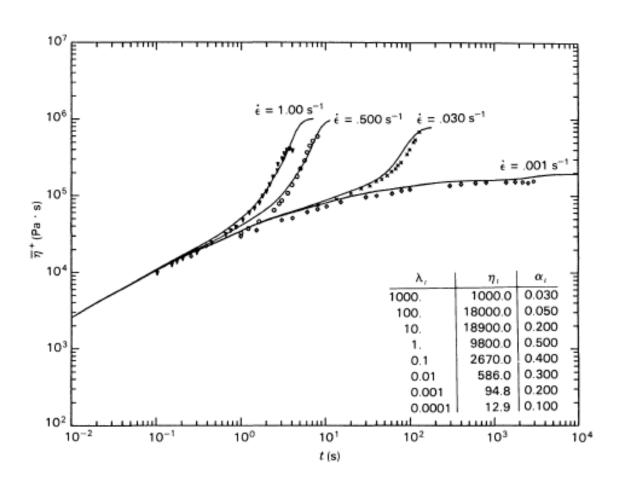
Steady Extensional Viscosity

$$\frac{\overline{\eta}}{3\eta_o} = \frac{1}{6a} \left(3 + \frac{1}{\lambda \dot{\varepsilon}} \sqrt{1 - 4(1 - 2a)\lambda \dot{\varepsilon} + 4(\lambda \dot{\varepsilon})^2} - \sqrt{1 + 2(1 - 2a)\lambda \dot{\varepsilon} + (\lambda \dot{\varepsilon})^2} \right)$$



Startup elongational Viscosity: η⁺



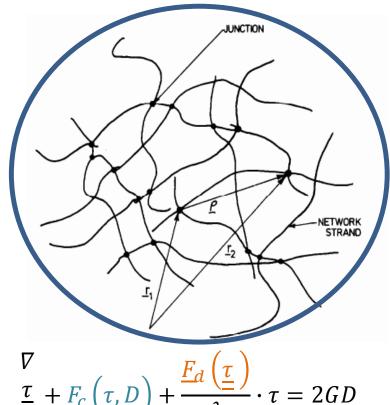


Comparison of ñ+ calculated by an 8-mode Giesekus model with experimental data for a low-density polyethylene melt



Phan-Tien & Tanner (PPT) model (based on network theory)

Typical network of polymer solutions



$$\frac{\nabla}{\underline{\tau}} + \underline{F_c} \left(\underline{\underline{\tau}}, \underline{\underline{D}}\right) + \frac{\underline{F_d} \left(\underline{\underline{\tau}}\right)}{\lambda} \cdot \underline{\underline{\tau}} = 2G\underline{\underline{D}}$$

$$V = \underline{\underline{\tau}} - \underline{\underline{D}} \cdot \underline{\underline{\tau}} - \underline{\underline{\tau}} \cdot \underline{\underline{D}}^T$$

 $\lambda = \eta/G$ is the relaxation time, ∇ over a variable indicates the upper convected time-derivative

 \underline{F}_{C} introduces non-affine motion of the polymer strands \underline{F}_d correlates with the creation and the destruction of junctions between the strands

Affine motion: The deformation characterizing the material at the macroscopic level is similar to its microscopic motion



The Phan Tien Tanner (PPT) model: the functions

Comments:

- The parameter $0 \le \xi \le 2$ alters the time derivative.
- For the limits, $\xi = 0$ and $\xi = 2$, the upper and lower convected time derivative are obtained.
- With $\xi=1$ the co-rotational time derivative results

$$\underline{F_c}\left(\underline{\underline{\tau}},\underline{\underline{D}}\right) = \underline{\xi}\underline{\underline{D}}\cdot\underline{\underline{\tau}} - \underline{\xi}\underline{\underline{\tau}}\cdot\underline{\underline{D}}^T$$

 In general the functional dependence is such that it accelerates stress decay rate at higher stresses and approaches zero at least quadratically when strains (i.e. stress divided by the modulus) approach zero. • <u>F</u>_d or f, the relaxation time of the model is made a non-linear function of the extra stress tensor scaled with a modulus.

$$\underline{F_d}(\underline{\underline{\tau}}) = \exp(\varepsilon/\mathsf{G}\,\mathsf{I}_{\tau})$$

Predicts a maximum in the elongational viscosity before reaching extensional thinning at higher elongational rates

$$\underline{F_d}(\underline{\tau}) = 1 + \varepsilon/G I_{\tau}$$

 Predicts extensional thickening behavior after which a plateau is reached at higher elongational rates



e−PPT model: material functions

Predicts:

- Shear thinning behavior for shear viscosity and normal stress difference
- The elongational viscosities become bounded.
- For ξ=0, the second normal stress difference becomes zero.

Limitations:

- For $\xi \neq 0$ spurious oscillations are predicted during start-up of shear flow.
- When ξ=0, similar predictions are obtained as the Giesekus model and no overshoot in the viscometric functions is predicted for start-up of shear

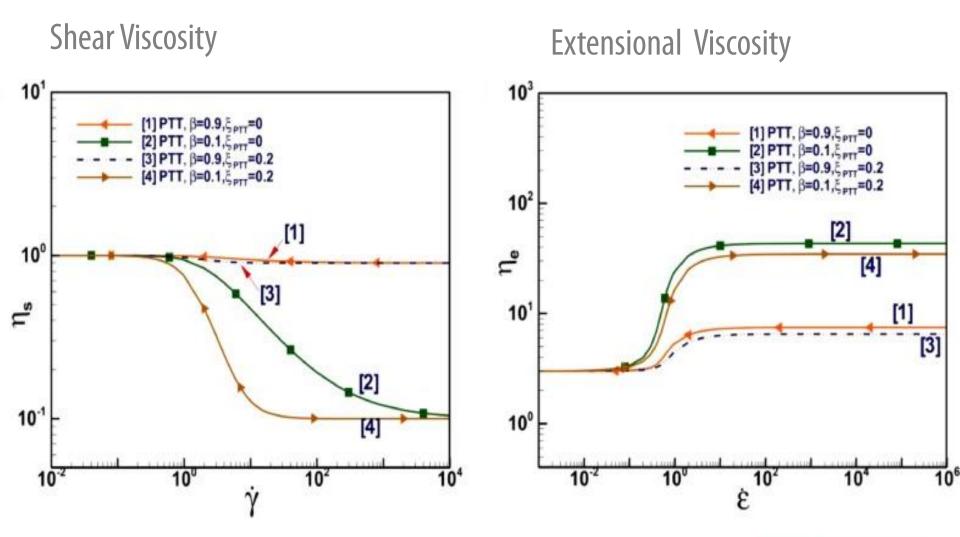
$$\begin{split} &\eta_s = \beta \eta_0 + \frac{\eta_0 (1-\beta)}{f}, \\ &N_1 = \frac{2\eta_0 (1-\beta)\lambda_1 \dot{\gamma}^2}{f^2}, \\ &N_2 = -\frac{\eta_0 (1-\beta)\lambda_1 \dot{\gamma}^2 \xi}{f^2}, \\ &\eta_e = 3\beta \eta_0 + 3\eta_0 (1-\beta) \bigg[\frac{f}{f^2 - f \lambda_1 \dot{\varepsilon} - 2\lambda_1^2 \dot{\varepsilon}^2} \bigg]. \\ &N_2/N_1 = -\xi/2 \end{split}$$

Comments:

- The two parameters ξ , ε define the non-linear behavior.
- When $\varepsilon < \xi$ the behavior in shear flow is mainly determined by ξ , and ε serves to blunt the singularity in elongation that otherwise would be present.
- A single value of the slip parameter cannot fit both shear viscosity and first normal stress difference satisfactorily.



Material Properties for *e*−PPT



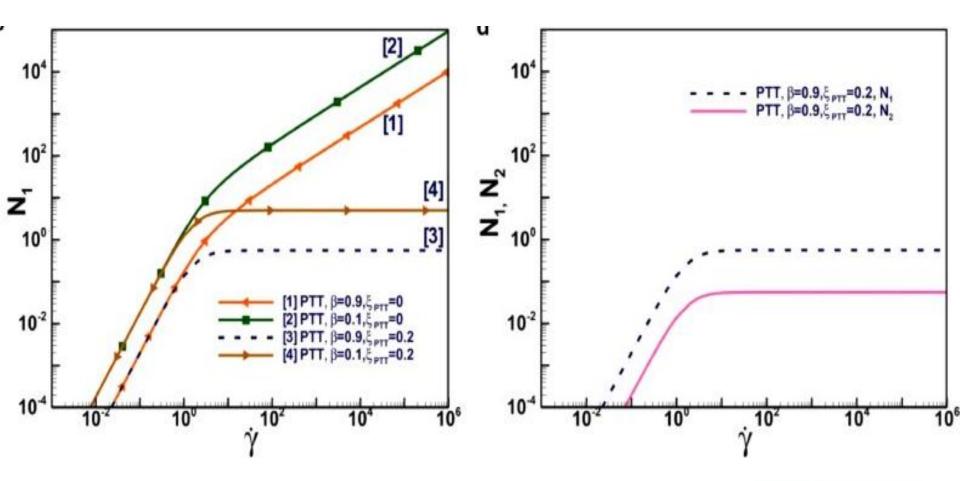
Material functions for PTT model with ε =0.04, ξ =0.0,0.2, β = 0.9, 0.1)



Material Properties for *e*−PPT

first normal stress-difference

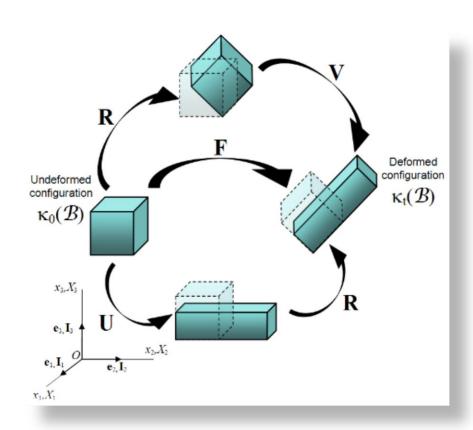
second normal stress-difference



Material functions for PTT model (ε =0.04, ξ =0.0,0.2), β = 0.9, 0.1



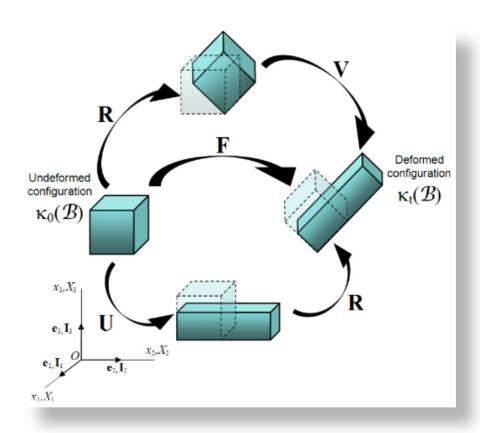




End of 4th lecture





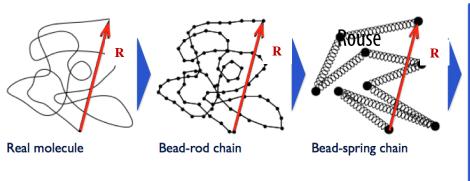


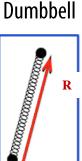
FENE Constitutive models

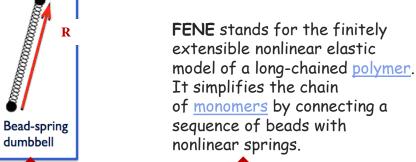


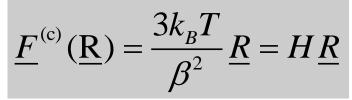
FENE Models











Hookean spring or Oldroyd-B model entropic spring

$$\underline{F}^{(c)}(\underline{\mathbf{R}}) = \frac{H\underline{R}}{1 - (\underline{R}/R_{\text{max}})^2}$$

Warner's model spring



FENE Models

$$\underline{\tau}_{=p} = \mathcal{G}\left(\left\langle \frac{\underline{R}\underline{R}}{1 - \underline{R}^2 / \underline{R}_{max}^2} \right\rangle - \underline{\underline{I}}\right)$$

$$\frac{\tau}{1 - \left\langle \underline{R} \underline{R} \right\rangle} - \underline{I}$$

$$\frac{1 - \left\langle \underline{R}^2 \right\rangle / \underline{R}_{\text{max}}^2}{1 - \left\langle \underline{R}^2 \right\rangle / \underline{R}_{\text{max}}^2}$$

$$\underline{\tau}_{=p} = G \left(\frac{\langle \underline{R}\underline{R} \rangle}{1 - \langle \underline{R}^2 \rangle / R_{\text{max}}^2} - \frac{R_{\text{max}}^2}{R_{\text{max}}^2 - 3} \underline{I} \right)$$

FENE

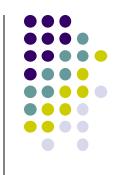
FENE-P

FENE-CR

$$G = nk_BT$$







$$\tau_{=p} = \frac{\eta_s cf(tr A)}{\lambda} = A$$

If the dumbbell model is considered to have a maximum attainable length L. The force of the dumbbell is given by Warner law.

$$\frac{\partial A}{\partial t} + \underline{v} \cdot \underline{\nabla} \underline{A} - (\underline{\nabla} \underline{v})^T \cdot \underline{A} - \underline{A} \cdot \underline{\nabla} \underline{v} = \frac{f(tr \underline{A})}{\lambda} (\underline{\underline{I}} - \underline{\underline{A}})$$

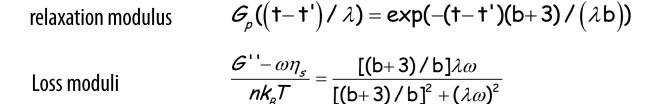
$$f(trA) = \frac{1}{1 - \frac{trA}{R_{max}^2}}$$

$$c = \frac{\eta - \eta_s}{\eta_s}$$
 Concentration



SAOS: relaxation modulus, G' & G"

FENE-P



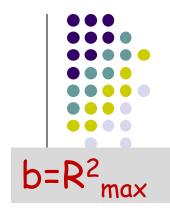
Storage moduli
$$\frac{\mathcal{G}'}{nk_{B}T} = \frac{\left(\lambda\omega\right)^{2}}{\left[\left(b+3\right)/b\right]^{2} + \left(\lambda\omega\right)^{2}}$$

FENE-CR

relaxation modulus
$$G_p((t-t')/\lambda) = \frac{b}{b-3} \exp(-(t-t')b/(b-3))$$

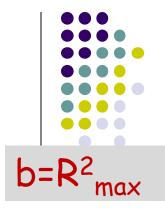
Loss moduli
$$\frac{G'' - \omega \eta_s}{nk_B T} = \frac{[b/(b-3)]^2 \lambda \omega}{[b/(b-3)]^2 + (\lambda \omega)^2}$$

Storage moduli
$$\frac{\mathcal{G}'}{nk_{B}T} = \frac{[b/(b-3)](\lambda\omega)^{2}}{[b/(b-3)]^{2} + (\lambda\omega)^{2}}$$

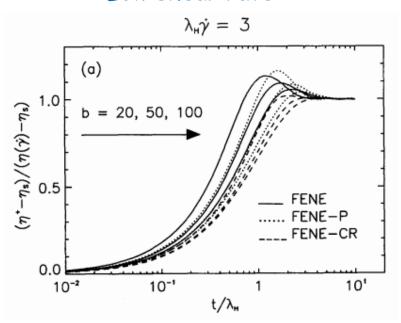




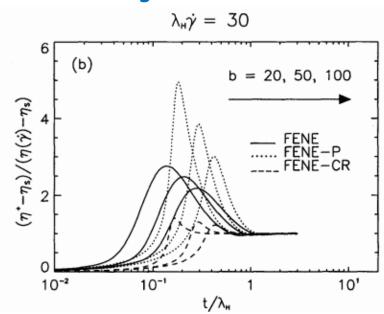
Startup shear flow: η +



Low shear rate



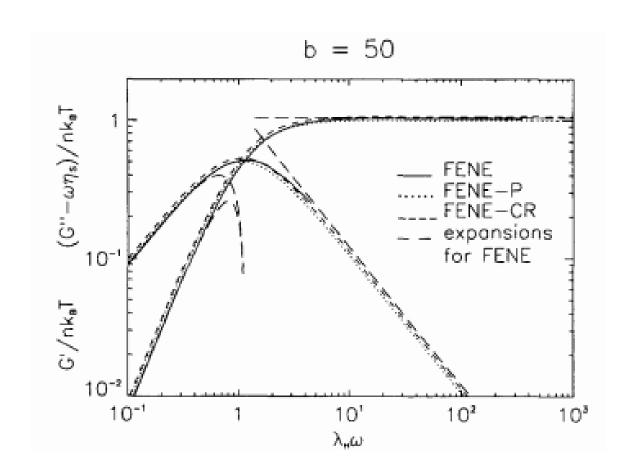
High shear rate

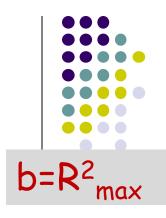


Time evolution of η^+ after inception of shear flow for FENE, FENE-P and FENE-CR



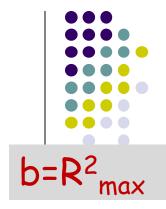
SAOS: G' & G"



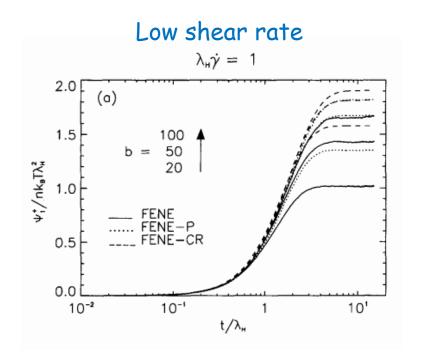


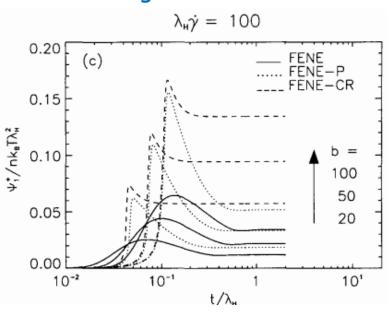


Startup shear flow: Ψ_1^+



High shear rate





Time evolution of Ψ_1^+ after inception of shear flow for FENE, FENE-P and FENE-CR

